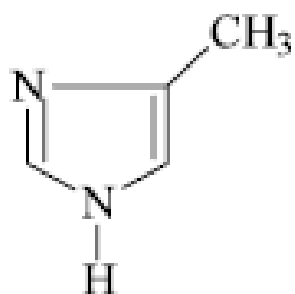
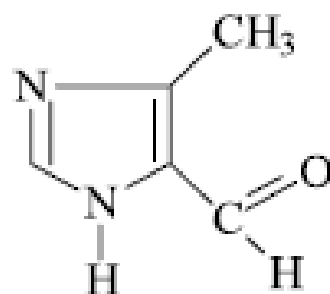


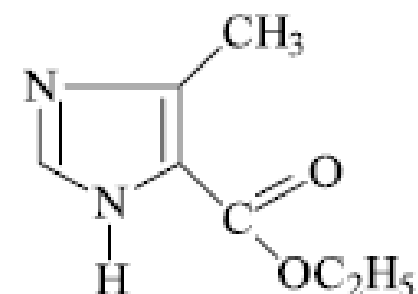
Imidazole  
*Inh1*



4-methylimidazole  
*Inh2*

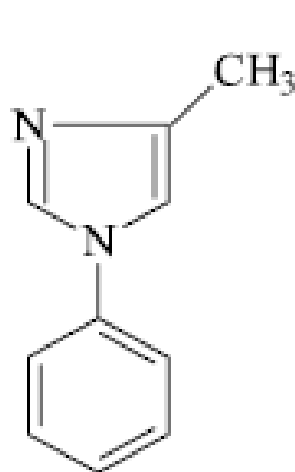


4-methyl-5-imidazole  
carbaldehyd

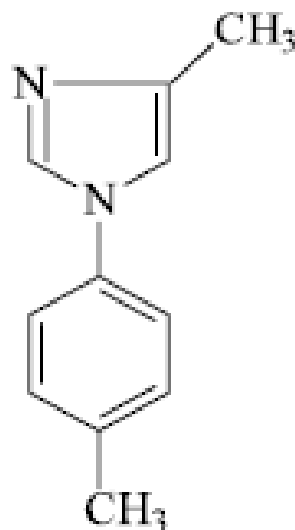


ethyl-4-methyl-5-  
imidazole carboxylate  
*Inh4*

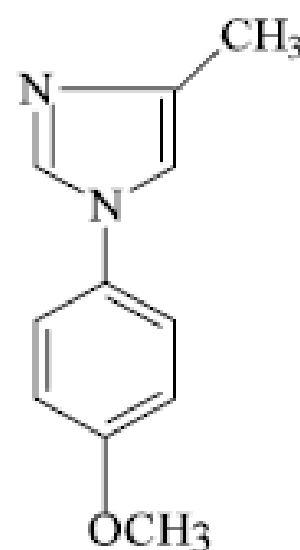
## CORROSION INHIBITORS



1-phenyl-4-methyl  
imidazole  
*Inh5*

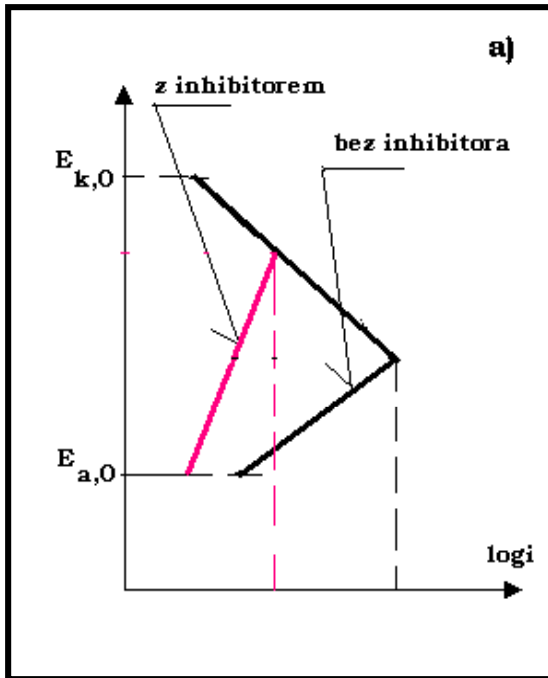


1-(p-tolyl)-4-methyl  
imidazole  
*Inh6*

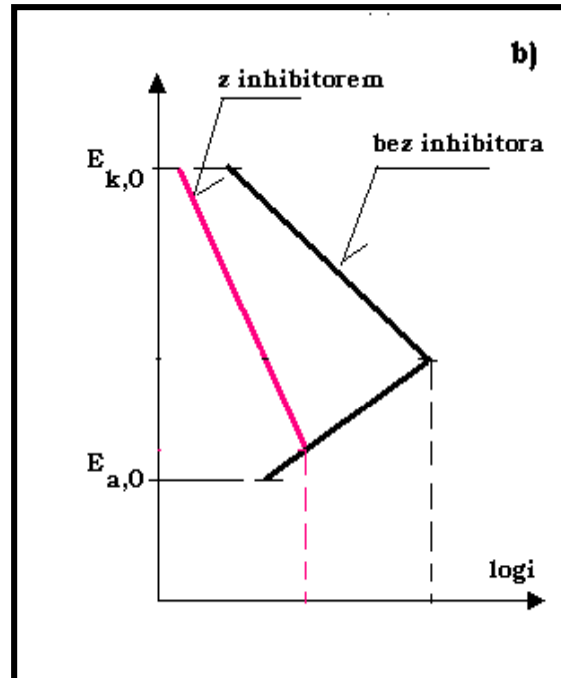


4-methyl-1(4-methoxyphenyl)  
imidazole  
*Inh7*

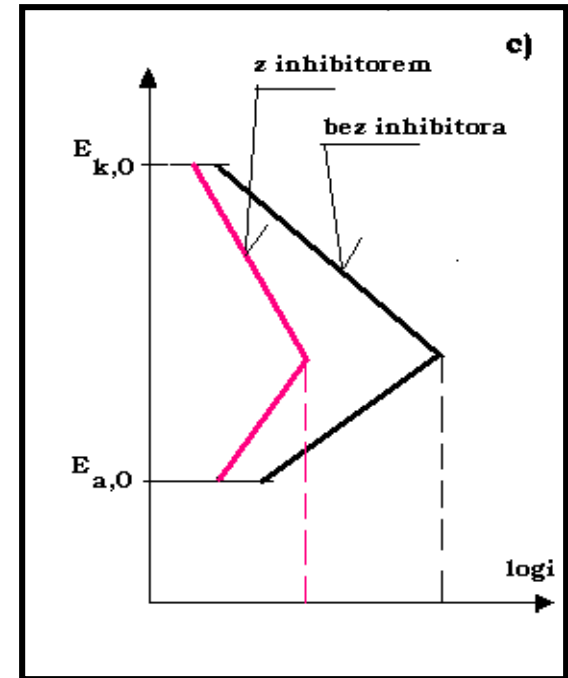
# Inhibitors



(a) **anodic inhibitors:**  
phosphates  
silicate compounds



(b) **Cathodic inhibitors**  
poly-phosphates  
 $\text{Ca}(\text{HCO}_3)_2$   
methylamino-phosphate



(c) **mixed anodic and cathodic inhibitors**  
amines  
selenides

# Inhibitors

## Types of Corrosion Inhibitors

### Organic

These materials are characterized by high molecular weight structures, incorporating nitrogen or phosphorous groups. They are usually highly polar molecules.

**Phosphate Esters**

**Phosphonates**

### Inorganic

Salts of some metals and amphoteric elements act as corrosion inhibitors. Quite often these materials have tenacious filmforming or passivation effects. In some instances, they react with the metal surface.

**Chromate Salts**

**Zinc Salts**

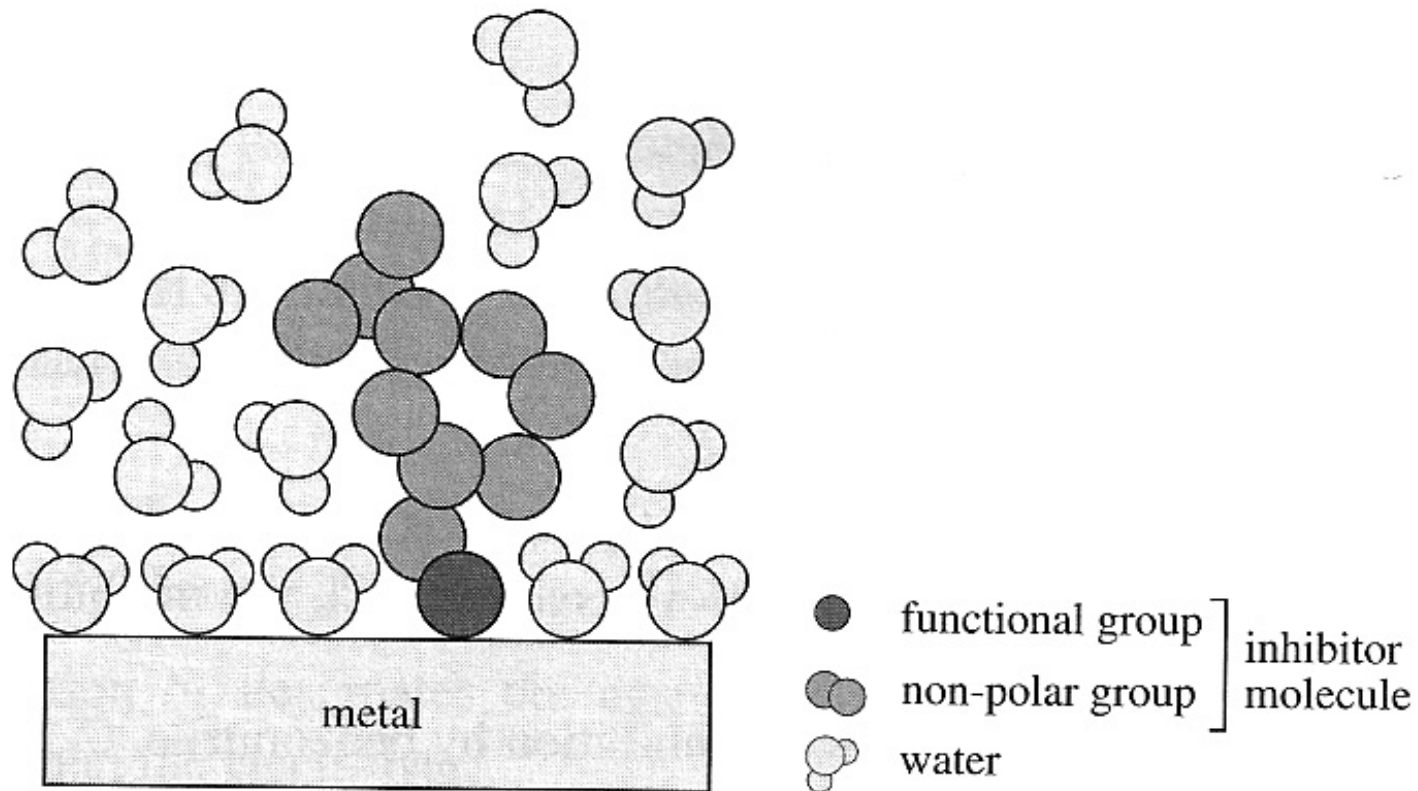
**Molybdate Compounds**

**Phosphates**

**Nitrite Salts**

**Silicate Compounds**

# Inhibitors



Adsorption of organic inhibitor onto a metal surface in aqueous environment

# Inhibitor efficiency

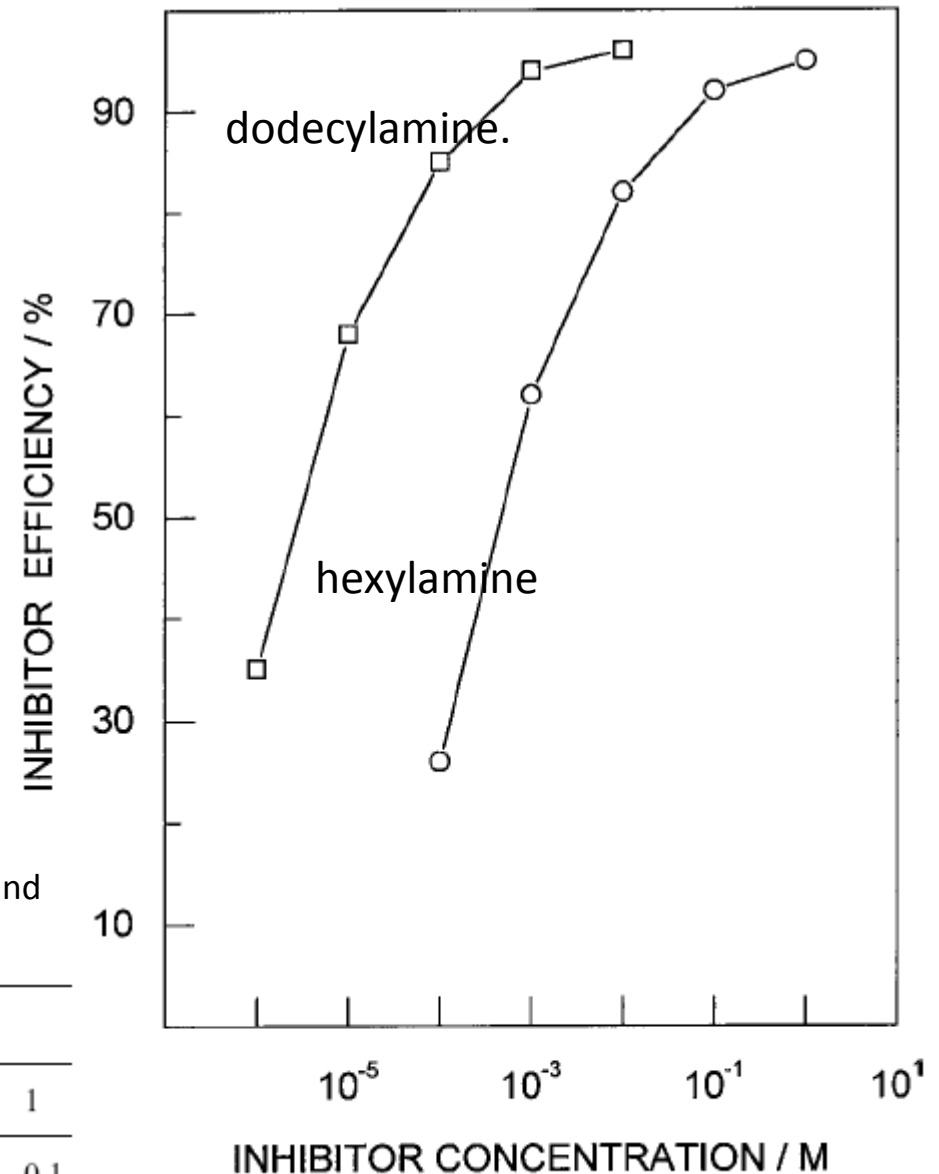
The percentage inhibitor efficiency is given by:

$$\frac{W_o - W_i}{W_o} \times 100$$

where  $W_o$  and  $W_i$  represent weight loss in the absence and presence of inhibitor, respectively.

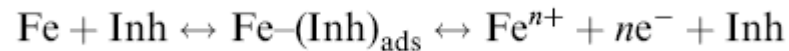
Mild steel corrosion rate in 2.0 M HCl in the presence and absence of inhibitor

Inhibitor concentration/M	Corrosion rate $\times 10^6/\text{kg m}^{-2} \text{s}^{-1}$							
	0	$10^{-6}$	$10^{-5}$	$10^{-4}$	$10^{-3}$	$10^{-2}$	$10^{-1}$	1
Hexylamine	2.8	–	–	2.1	1.1	0.5	0.2	0.1
Dodecylamine	2.8	1.8	0.9	0.4	0.2	0.1	–	–



## Mechanism of inhibition

According to Bockris and Drazic, the inhibition mechanism can be explained by the  $\text{Fe}\pm(\text{Inh})_{\text{ads}}$  reaction intermediates



This  $\text{Fe}-(\text{Inh})_{\text{ads}}$  intermediate forms an adsorption layer through the nitrogen atom of the inhibitor. The adsorption layer acts as a hindrance to the solution and enhances the protection of the metal surface.

The adsorption of an organic compound on the surface of a mild steel electrode is regarded as a substitutional adsorption process between the organic compound in the aqueous phase ( $\text{Org}_{\text{aq}}$ ) and the water molecules adsorbed on the mild steel surface ( $\text{H}_2\text{O}_{\text{ad}}$ )



where  $X$  is the size ratio, that is, the number of water molecules replaced by one organic molecule.

The degree of surface coverage  $\theta$  can be plotted as a function of the concentration of hexylamine or dodecylamine inhibitors in the hydrochloric acid solution. The value of  $\theta$  was calculated from the inhibitor efficiency relationship:

$$\theta = \frac{W_o - W_i}{W_o}$$

# Adsorption isotherm

Interaction between the organic compounds and metal surfaces

Temkin isotherm

$$\exp(f \cdot \theta) = k_{\text{ads}} \cdot C$$

Langmuir isotherm

$$\frac{\theta}{1 - \theta} = k_{\text{ads}} \cdot C$$

Frumkin isotherm

$$\frac{\theta}{1 - \theta} \cdot \exp(-2f \cdot \theta) = k_{\text{ads}} \cdot C$$

Freundlich isotherm

$$\theta = k_{\text{ads}} \cdot C$$

## Adsorption isotherm plots

The most commonly used substitutional isotherms:

Flory-Huggins  $kc = \frac{\theta}{X(1-\theta)^X}$  H.P. Dhar, B.E. Conway and K.M. Joshi, Electrochim. Acta 18 (1973) 789.

Dhar-Flory-Huggins  $kc = \frac{\theta}{e^{(X-1)}(1-\theta)^X}$  H.P. Dhar, B.E. Conway and K.M. Joshi, Electrochim. Acta 18 (1973) 789.

Bockris-Swinkels  $kc = \frac{\theta}{(1-\theta)^X} \frac{[\theta + X(1-\theta)]^{(X-1)}}{X^X}$  J. O'M. Bockris and D.A.J. Swinkels, J. Electrochem. Soc. 111 (1964) 736.

where  $X$  is the number of water molecules replaced by one molecule of organic compound,  $c$  is the inhibitor concentration and  $k$  is the equilibrium constant of the adsorption reaction given by:  $k_c = 1/55.5[\exp(-\Delta G_{\text{ads}}^0/RT)]$ .

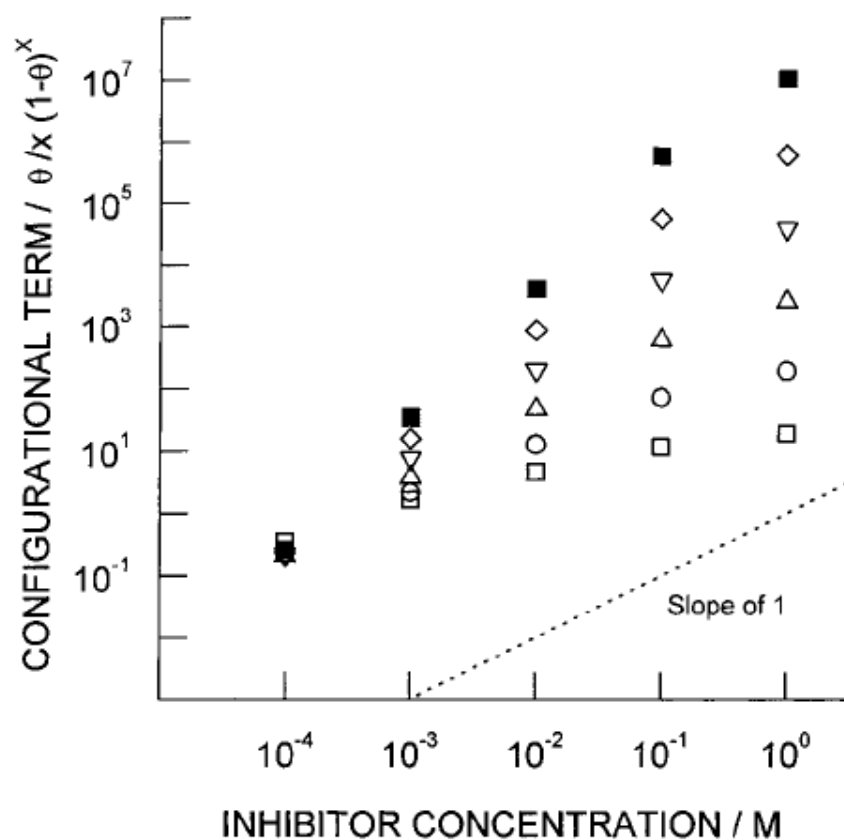
Equations at the top may be written as:

$$\log[f(\theta, X)] = \log c + \log k$$

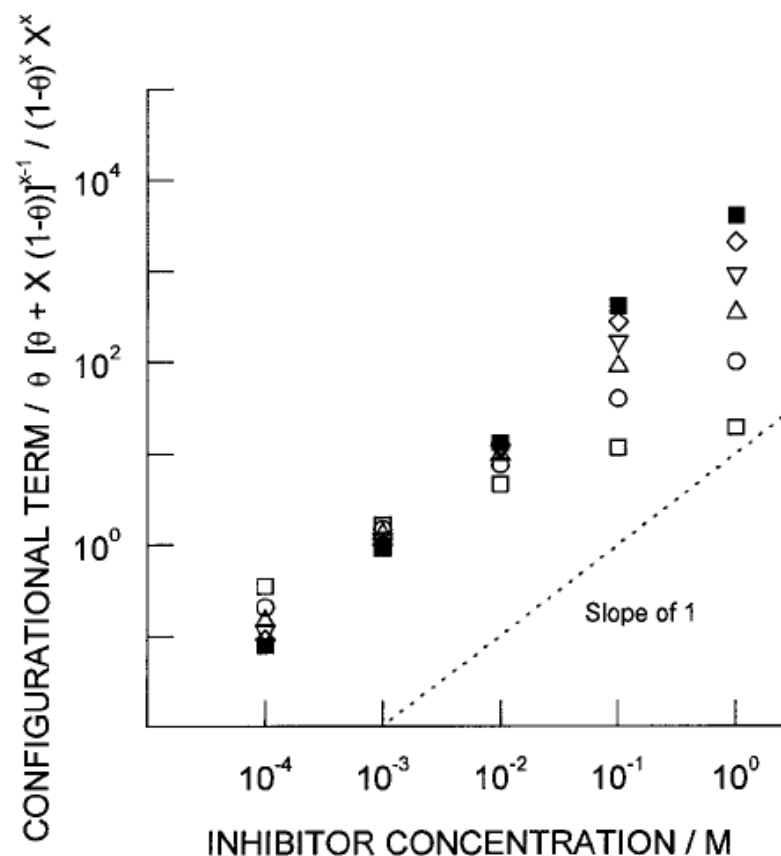
where  $f(\theta, X)$  is the configurational term, which depends essentially on the physical model and assumptions underlying the derivation of the isotherm .



A plot of  $\log f(\theta, X)$  against  $\log c$ , for a specified value of  $X$ , is a straight line with a slope of unity, and the ordinate axis intercept gives the  $\log k$  value.

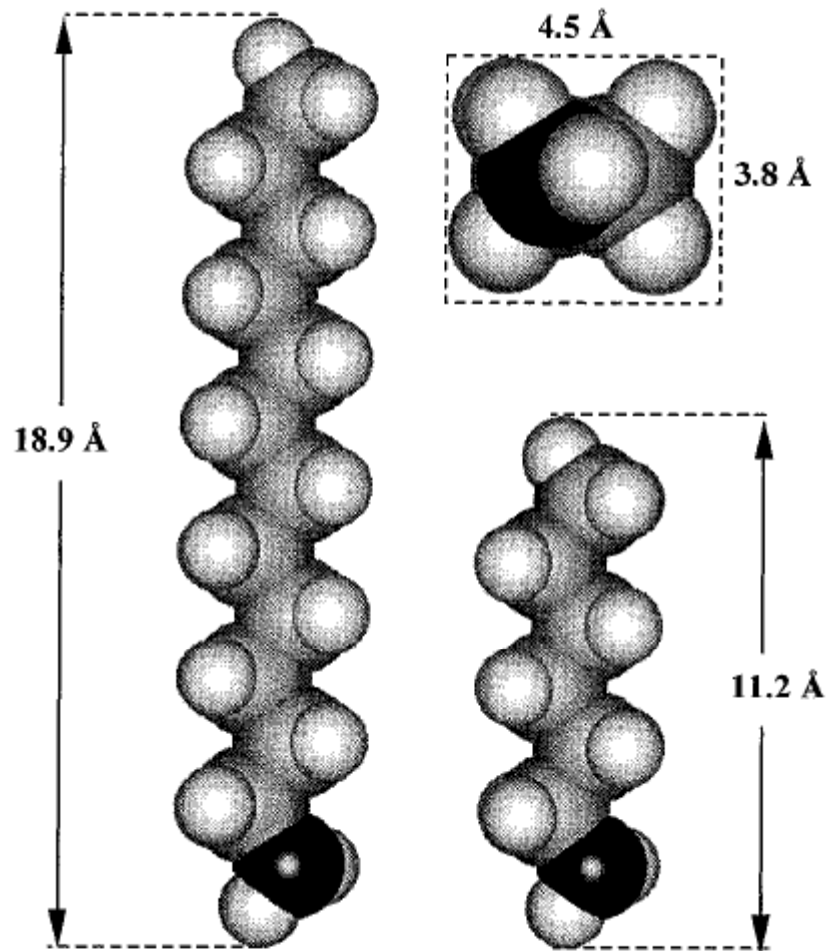


Flory-Huggins isotherm plot



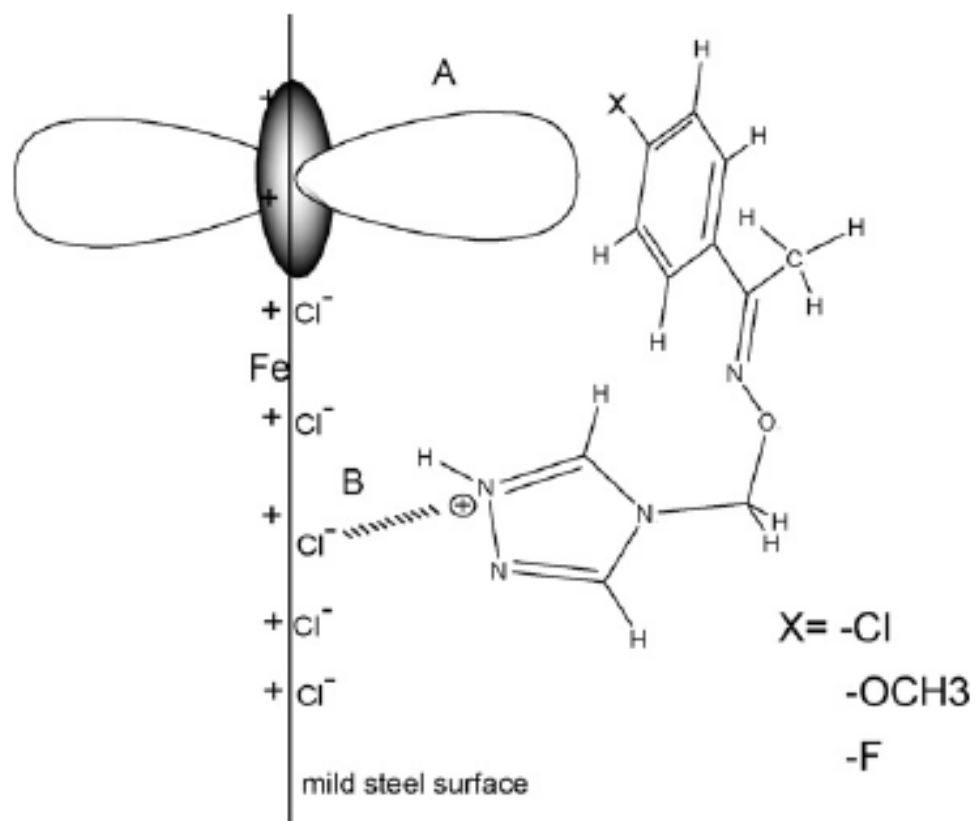
Bockris-Swinkels isotherm plot

for mild steel in 2.0 M HCl acid solution, at 298 K, for 24 h experimentation and for values of  $X$  up to 6. Key: (□)  $X = 1$ , (○)  $X = 2$ , (△)  $X = 3$ , (▽)  $X = 4$ , (◇)  $X = 5$  and (■)  $X = 6$ .



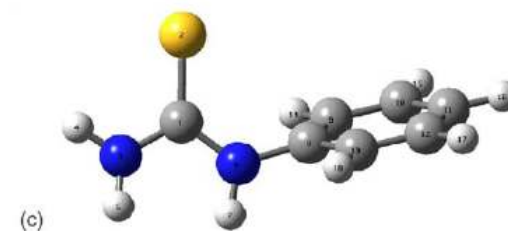
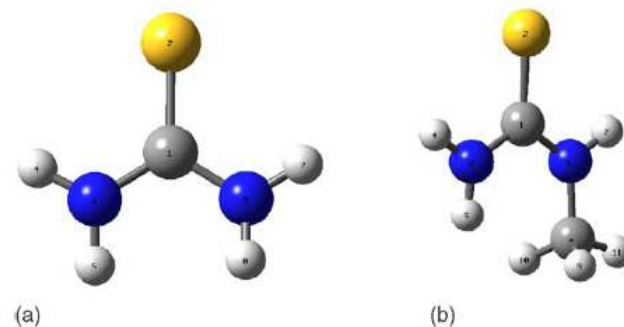
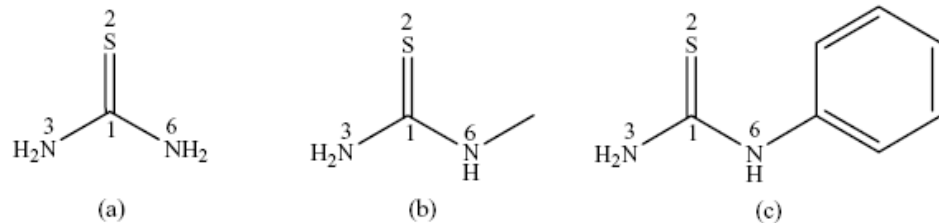
*Fig. 5.* Front view of hexylamine (bottom right) and dodecylamine (left) molecules adsorbed onto mild steel electrode. Top view (upper right corner).

the area occupied by a vertically-oriented adsorbed hexylamine/dodecylamine molecule is about  $17 \text{ \AA}^2$  (the projected area of a rectangle surrounding a molecule), as compared with  $50 \text{ \AA}^2$  for hexylamine and  $85 \text{ \AA}^2$  for dodecylamine for the horizontal orientations



Two kinds of adsorption can be acting on steel surface:

Type A means the interaction between the benzene ring, C N and the vacant, low energy d-orbitals of Fe surface atoms, this process is called chemisorption. Type B shows the electrostatic interaction between the positively charged N atom and the negatively charged Cl<sup>-</sup> on mild steel surface, which is regard as physisorption.



M. Özcan, İ. Dehri, M. Erbil, Applied Surface Science 236 (2004) 155–164

Impedance parameters and inhibition efficiency for the corrosion of mild steel in 0.1 M H<sub>2</sub>SO<sub>4</sub> with and without addition of various concentrations of TU, MTU and PTU

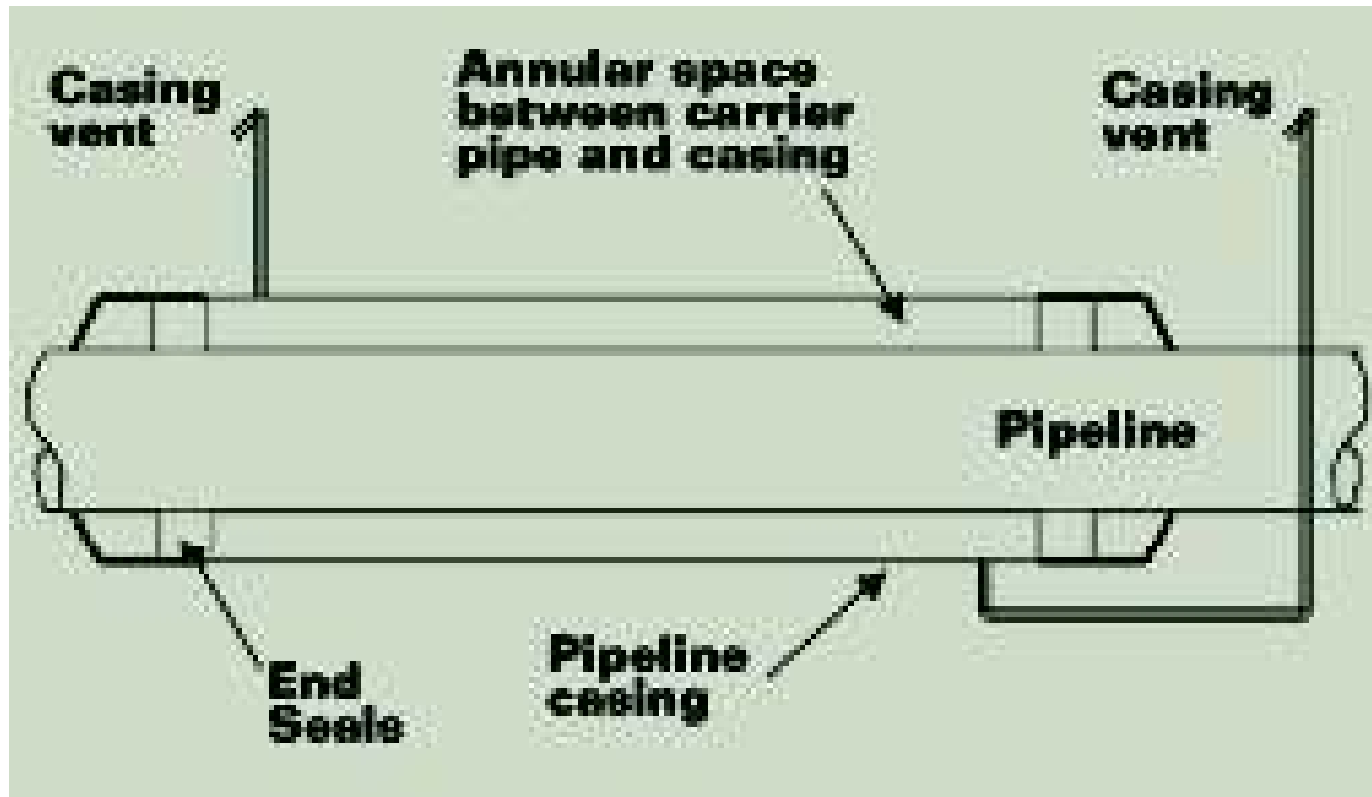
Molecule	Inhibition concentration (M)	$E_{corr}$ vs. Ag/AgCl (V)	$R_p$ ( $\Omega$ ) <sup>a</sup>	$R_p$ ( $\Omega$ ) <sup>b</sup>	$C_{dl}$ ( $\mu$ F)	IE (%)
Blank	–	–0.526	36	25	137	–
TU	$10^{-4}$	–0.532	66	52	53.3	51.9
	$10^{-3}$	–0.521	224	192	39.0	87.0
	$10^{-2}$	–0.511	376	351	31.6	92.9
MTU	$10^{-4}$	–0.520	62	51	32.0	51.0
	$10^{-3}$	–0.505	293	330	18.8	92.4
	$10^{-2}$	–0.494	577	563	16.2	95.6
PTU	$10^{-4}$	–0.520	62	49	86.5	49.0
	$10^{-3}$	–0.497	820	788	7.86	96.8
	$10^{-2}$	–0.454	905	896	8.37	97.2

<sup>a</sup>  $R_p$  from polarisation resistance measurements.

<sup>b</sup>  $R_p$  from Nyquist diagrams.

# Application of corrosion inhibitors

A vapor phase corrosion inhibitor is used to protect the annular space in road crossings.



Below ground road casing. Annular space between the casing and the carrier pipe can be protected with a VpCI or filled to mitigate corrosion in the annular space.

# Application of corrosion inhibitors

<b>Engine coolants</b>	<b>Sodium chromate</b>	<b>Fe, Pb, Cu, Zn</b>	<b>0.1-1%</b>
<b>..</b>	<b>Sodium nitrite</b>	<b>Fe</b>	<b>0.1-1%</b>
<b>..</b>	<b>Borax</b>	<b>..</b>	<b>1%</b>
<b>Glycol/water</b>	<b>Borax + MBT</b>	<b>All</b>	<b>1% + 0.1%</b>
<b>Oil field brines</b>	<b>Sodium silicate</b>	<b>Fe</b>	<b>0.01%</b>
<b>..</b>	<b>Quaternaries</b>	<b>..</b>	<b>10-25 ppm</b>
<b>..</b>	<b>Imidazoline</b>	<b>..</b>	<b>10-25ppm</b>
<b>Seawater</b>	<b>Sodium silicate</b>	<b>Zn</b>	<b>10 ppm</b>
<b>..</b>	<b>Sodium nitrite</b>	<b>Fe</b>	<b>0.5%</b>
<b>..</b>	<b>Calcium bicarbonate</b>	<b>All</b>	<b>pH dependent</b>
<b>..</b>	<b>Sodium phosphate monobasic + Sodium nitrite</b>	<b>Fe</b>	<b>10 ppm + 0.5%</b>

<b>System</b>	<b>Inhibitor</b>	<b>Metals</b>	<b>Concentration</b>
<b>Acids</b>			
<b>HCl</b>	<b>Ethylaniline</b>	<b>Fe</b>	<b>0.5%</b>
<b>..</b>	<b>Mercaptobenzotriazole</b>	<b>..</b>	<b>1%</b>
<b>..</b>	<b>Pyridine + phenylhydrazine</b>	<b>..</b>	<b>0.5% + 0.5%</b>
<b>..</b>	<b>Rosin amine + ethylene oxide</b>	<b>..</b>	<b>0.2%</b>
<b>Sulfuric</b>	<b>Phenylacridine</b>	<b>..</b>	<b>0.5%</b>
<b>Phosphoric</b>	<b>Sodium iodide</b>	<b>..</b>	<b>200 ppm</b>
<b>Others</b>	<b>Thiourea</b>	<b>..</b>	<b>1%</b>
<b>..</b>	<b>Sulfonated castor oil</b>	<b>..</b>	<b>0.5-1.0%</b>
<b>..</b>	<b>Arsenic Oxide</b>	<b>..</b>	<b>0.5%</b>
<b>..</b>	<b>Sodium arsenate</b>	<b>..</b>	<b>0.5%</b>
<b>Water</b>			
<b>Potable</b>	<b>Calcium bicarbonate</b>	<b>Steel, cast iron</b>	<b>10 ppm</b>
<b>..</b>	<b>Polyphosphate</b>	<b>Fe, Zn, Cu, Al</b>	<b>5-10 ppm</b>
<b>..</b>	<b>Calcium hydroxide</b>	<b>Fe, Zn, Cu</b>	<b>10 ppm</b>
<b>..</b>	<b>Sodium silicate</b>	<b>..</b>	<b>10-20 ppm</b>
<b>Cooling</b>	<b>Calcium bicarbonate</b>	<b>Steel, cast iron</b>	<b>10 ppm</b>
<b>..</b>	<b>Sodium chromate</b>	<b>Fe, Zn, Cu</b>	<b>0.1%</b>
<b>..</b>	<b>Sodium nitrite</b>	<b>Fe</b>	<b>0.05%</b>
<b>..</b>	<b>Sodium phosphate monobasic</b>	<b>..</b>	<b>1%</b>
<b>..</b>	<b>Morpholine</b>	<b>..</b>	<b>0.2%</b>
<b>Boilers</b>	<b>Sodium phosphate monobasic</b>	<b>Fe, Zn, Cu</b>	<b>10 ppm</b>
<b>..</b>	<b>Polyphosphate</b>	<b>..</b>	<b>10 ppm</b>
<b>..</b>	<b>Morpholine</b>	<b>Fe</b>	<b>variable</b>
<b>..</b>	<b>Hydrazine</b>	<b>..</b>	<b>O2 scavenger</b>
<b>..</b>	<b>Ammonia</b>	<b>..</b>	<b>neutralizer</b>
<b>..</b>	<b>Octadecylamine</b>	<b>..</b>	<b>variable</b>